

# **Distributed Generation in Industrial Facilities**

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# Presentation Outline

- **Distributed Generation**
- **Tri-generation**
- **Case study**
- **Conclusion**



# Distributed Generation

Embedded generators generating electricity primarily for on-site consumption and not to compete with gencos in the electricity market

## Applications:

- Combined heat and power
- Emergency/Temporary power
- Price hedging

# Tri-gen Installations Supported by NEA

Installations		Electricity Output (kWe)	Thermal Output (kWt)	Cooling Output (kWt)
Mirco-turbine tri-gen system	Design	56	310	582
	Operating	38	122	388
Town gas fired gas engine with burner	Design	655	339 + 556 (from burner)	-
	Operating	570	473	-

# Tri-gen Installations Supported by NEA

Installations		Electricity Output (kWe)	Steam Output (MT/h)	Cooling Output (kWt)
Natural gas fired tri-gen plant 1	Design	5,000	12.7	4,500
	Operating	4,600	11.5	4,750
Natural gas fired tri-gen plant 2	Design	10,000	24.1	14,068
	Operating	9,100	24	17,057

# Case Study

## *Proposed Tri-gen System*

- Electricity demand about 4MW
- Steam demand average 2.5 t/hr at 8 bar
- Hot water requirement of 350 kW at 60 deg C
- Cooling > 6000kWt

# Generator sized to meet hot water demand

## Tri-generation System

### Primary energy (Input)

	% PE	Power (MW)	Consumption per year (MWh)	NG Cost (\$\$)	CO2 emission (tonnes)
Natural Gas	100%	4.39	34,600	2,430,000	6,370

### Energy Production

Energy (Output)	% PE	Power (MW)	COP/Extra Usage (MW)	Yearly production (MWh)	
Electricity	41%	1.8	0.16	12,900	
Steam	18%	0.8		6,300	
Chilled water	16%	0.7	0.7	3,850	
Hot water	8%	0.34		2,700	
Losses	17%	0.75		5,950	
	100%	4.39			

## Conventional System (separate production)

	Consumption (MWh/year)	Efficiency/COP	Energy (MWh/year)	Cost (\$\$)	CO2 emission (tonnes)
Steam	6,300	90%	7,000	492,100	1,300
Electricity	12,900	1	12,900	2,751,500	6,920
Chilled water	3,850	5	770	164,400	410
Hot water	2,700	98%	2,700	192,000	50
Total				3,600,000	9,130

# Generator sized to meet steam Demand

## Tri-generation System

### Primary energy (Input)

	% PE	Power (MW)	Consumption per year (MWh)	NG Cost (\$\$)	CO2 emission (tonnes)
Natural Gas	100%	8.78	69,200	4,862,000	12,740

### Energy Production

Energy (Output)	% PE	Power (MW)	COP/Extra Usage (MW)	Yearly production (MWh)	
Electricity	41%	3.60	0.16	27,100	
Steam	18%	1.60		12,600	
Chilled water	16%	1.40	0.7	7,700	
Hot water	4%	0.34		2,700	
Losses	21%	1.84		14,500	
	100%	8.78			

## Conventional System (separate production)

	Consumption (MWh/year)	Efficiency/COP	Energy (MWh/year)	Cost (\$\$)	CO2 emission (tonnes)
Steam	12,600	90%	14,000	984,000	2,580
Electricity	27,100	1	27,100	5,771,000	14,500
Chilled water	7,700	5	1,550	328,800	830
Hot water	2,700	98%	2,700	192,100	500
Total				7,275,900	18,410



# Comparison

	Sized to meet hot water demand	Sized to meet steam demand
Energy Cost saving (S\$/yr)	1,170,000	2,413,900
CO2 Reduction (Tonnes/yr)	2,760	5,670
Annual O&M Cost (S\$/yr)	200,000	200,000
CAPEX Budget Forecast (S\$)	5,280,000	10,560,000
Payback Period (years) (Including O&M cost)	5.4	4.8
Payback Period (years) (Excluding O&M cost)	4.5	4.4

# Observations

- Technology is an integral part of the evaluation
  - Micro-turbine vs gas turbine vs gas engine
- There are multiple utilities to evaluate
  - Steam (heat), hot water, chilled water, dehumidification, electricity
- Each combination has implications on cost, savings, flexibility, carbon footprint, primary energy requirements

# Observations

- Selection process is complex and needs to be matched to facility specific requirements
- Life-cycle analysis / cost-benefit analysis is equally complex and requires greater sophistication and detailed sensitivity analysis
  - Spark spread may vary over time, so ability to hedge market electricity prices will also vary
  - Offsetting cost of producing steam and other utilities has a bearing on overall project economics
  - Once investment is sunk, marginal operating cost considerations take over

# Observations

- **Sizing the plant is often key**
  - **Steam (heat) demand as sizing parameter appears most critical for best project economics and lowest carbon emissions**
  - **If heating demand varies, storage options should be considered to smooth requirements for better plant utilisation; same cannot be said with certainty for chilled water**
  - **Relationship between desired steam parameters, technology, costs not well understood**

# Observations

- **Confusion arises when overall thermodynamic efficiency is a consideration in decision making**
- **Meeting cooling requirements, i.e. chilled water, dehumidification, usually turn out to be of incidental concern**
- **Same can be said for hot water**
- **Sizing for electricity requirement results in waste heat not being fully utilised and higher carbon emissions**

# Observations

- All parasitic loads must be considered in evaluations
  - Auxiliary pumps, fans, gas booster pumps, etc
- Suitability of town gas for cogen or trigen is questionable – small spark spread, difficult fuel to manage
- Evaluate all this while keeping an eye on the electricity market regulatory environment

# Thank you

Information on  
energy efficiency initiatives of E<sup>2</sup>PO is available at  
[www.e2singapore.gov.sg](http://www.e2singapore.gov.sg)